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USE OF NATIVE CELLULOLYTIC ENZYMES FROM ECUADOR, IN THE ENZYMATIC HYDROLYSIS FOR THE ETHANOL PRODUCTION

USO DE ENZIMAS CELULOLÍTICAS NATIVAS DE ECUADOR, EN LA HIDRÓLISIS ENZIMÁTICA PARA LA PRODUCCIÓN DE ETANOL

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ABSTRACT

This study shows the use of cellulolytic enzymes *Bacillus sp.* in enzymatic hydrolysis process and their use in the production of second-generation ethanol. For doing this, The Plackett-Burman method was used to discard variables that do not influence the enzymatic hydrolysis process, and subsequently to adjust the model using the factorial optimization design Box-Hunter 2^{5-2} . Once the conditions of the experiments in the enzymatic hydrolysis process were optimized, the best testwas selected considering the highest glucose yield per 100g bagasse. The fermentative stage was also analyzed, resulting in a possibility of producing 1 liter of second-generation ethanol per 12.83kg bagasse and 77.9 liters per ton of bagasse.

Keywords: Enzyme cocktail; enzyme production; second-generation ethanol.

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RESUMEN

El presente estudio muestra el uso de enzimas celulolíticas de *Bacillus sp* en el proceso de hidrólisis enzimática y su empleo en la producción de etanol de segunda generación. Se emplea el método de Plackett-Bürman, para descartar variables que no influyen en el proceso de hidrólisis enzimática, para así posteriormente ajustar el modelo y utilizar el diseño de optimización factorial de Box-Hunter2⁵⁻². Una vez optimizadas las condiciones de los experimentos en el proceso de hidrólisis enzimática, se seleccionó el mejor ensayo considerando el rendimiento más alto de glucosa por 100g de bagazo, y se analizó la etapa fermentativa, obteniendo como resultado que se producirá 1 litro de etanol de segunda generación por cada 12,83kg de bagazo y 77,9 litros por cada tonelada de bagazo.

Palabras clave: cocktail enzimático; producción de enzimas; etanol.

1. INTRODUCTION

Lignocellulosic waste material as an energy resource has become more important, due to the fact that some energy crises have been generated globally as a result of fluctuations in oil prices over the last fifty years (González et al., 2008).

This circumstance has led to the search for more suitable raw material for the production of fuels as an alternative to traditional sources, originated from fossil materials, coupled with the environmental deterioration, caused by toxic compounds generated during their combustion (Gualteros, 2011). Therefore, the search and use of new resources and chemicals is required and this is where biomass and particularly lignocellulosic biomass, is revealed as a very promising source of renewable energy and chemicals generation in the world (Alvarez et al., 2012).

The ethanol produced by sources of lignocellulosic material has become an alternative use to the waste generated in the sugarcane industry, being this process with high accessibility to the raw material, since no significant advantage to bagasse is given, and the cost thereof is relatively low (Guarnizo et al., 2009).

One of the main challenges of the marketing process for obtaining ethanol from lignocellulosic materials is to make the process economically sustainable (Mesa, 2010).

To evaluate the effectiveness of new microbial cellulolytic enzymes in respect to glucose production from vegetable waste, an ideal way is experimentation using pilot schemes in which the combination of the tests of an experiment is proposed.

The efforts in developing methods to find optimal conditions, have a contribution for the work of (Box and Hunter, 1961), in which all the factors of the study are varied without having to make all possible experiments, called fractional factorial design; achieving the main objectives of the experimental design of reducing the number of tests and obtaining more information.

Considering that the production of microbial enzyme cocktail produced at laboratory scale can be carried on an industrial scale, by understanding the conditions required by the hydrolysis process; some research are aimed at finding new microorganisms within the existing diversity or even create new microorganisms at laboratory scale. In this research a microorganism that has been collected in a craft factory of *panela (It is a*

sweetener derived from the sugar cane juice) production in Balzapamba is used, which has shown interesting cellulolytic activities (Salvador, 2017). From this analysis, the research has set the overall aim: to determine the best conditions of enzymatic hydrolysis of Bacillus bacteria, native to Ecuador, that is going to be used in the production of second-generation ethanol.

2. MATERIALS AND METHODS

2.1. Pretreatment of lignocellulosic material

2.1.1. Raw material

Sugar cane bagasse (60% w/w) was collected in Puyo-Ecuador. Then it was triturated until a size of 1.5 mm for its use in the experiments. The composition of the material in relation to the percentage of dry matter was glucan, 49.0%; xylan, 15.6%; 27.24% lignin.

2.1.2. Acid hydrolysis

This treatment was applied to 500 grams of bagasse, with 1.25% sulfuric acid (w/w) and a relation of bagasse and sulfuric acid 1:10. This was put in the autoclave for 40 minutes at 134 °C and 2 atm of pressures. After this, the liquor was collected, and bagasse was pretreated with water in a proportion 1:1, then filtered and moved to the next pretreatment.

2.1.3. Hydrolysis basic-organosolv

30% ethanol and 7% NaOH, dry fiber concentration was added to the filtrate. The NaOH bagasse ratio is 1:7 and was placed in the autoclave at 175 °C for 90 minutes. The pretreated solid was washed with water to remove the ethanol and alkali, to pass to a drying stage of four hours at 40 °C, later the sample was analyzed to see the remnants of glucose, xylose and lignin content (Sidiras and Salapa, 2015).

2.2. Enzymatic hydrolysis of bagasse

According to the qualitative and quantitative tests, two microorganisms were chosen and evaluated for the enzymatic hydrolysis of bagasse, the hydrolysis was performed with 5% pretreated bagasse, 1 ml of citrate buffer (pH 4.8) and 0.1 g of Tween 80 surfactant. The enzymatic crude was obtained by filtering the medium in which the microorganism had grown. 2 ml of enzymatic cocktail were placed and measurements of the established conditions were made according to (Salvador et al., 2018).

2.3. Experimental design

To achieve these objectives, the possibility of combining the Plackett-Bürman method (González et al., 1986) of multivariable systems with partial recesses for polynomials of the first degree of the Box-Hunter method (1961). The matrix for rotational designs was completed, taking full advantage of all the runs made and calculating a quadratic equation, as appropriate. The combination of the Plackett-Bürman method with that of Box-Hunter has already been applied in hydrolysis research with enzymes, obtaining satisfactory results (Salvador et al., 2018) that have served for the identification of some stages and systems of the process.

2.3.1. The method of Plackett-Bürman

The method of Plackett-Bürman (Plackett and Bürman, 1946) is based on a highly fractional factorial design that studies all the possible variables that affect the system, and manages to determine which the most influential ones are. It is considered an initial program to study processes that have a high number of variables and should continue research in the experimental region, after discarding non-influential variables, with a more rigorous plan, with the aim of finding a more appropriate model.

To apply the method, Isaacson (1970) recommends that additional experiments to estimate the standard error and the variance, due to experimental errors, interactions or quadratic effects; that is why false variables are included in the experimental plan.

2.3.2. Box-Hunter optimization design (Box and Hunter, 1961).

All the information provided by a 2^n plan may not be of interest, since interactions of a higher order are usually negligible. In these cases, it is advisable to use the fractional plans, as they are useful:

- a. when there are negligible interactions,
- b. in the determination of significant variables,
- c. in sequential investigations where the results lead to modify our experiences and
- d. when the influences of several factors can be described by a single main effect.

With the new conditions that influence the experiment, we proceeded to measure glucose yield, taking into account the results of the Box-Hunter experimental design. For the production of second-generation ethanol from the results obtained in glucose yield per 100g of bagasse, the experimental results of the fermentative stage (Hydrolysis and separate fermentation, HFS) and ethanol extraction were taken (Mesa, 2010).

3. RESULTS AND DISCUSSION

The best conditions of the enzymatic hydrolysis were determined starting from the experience reached by Salvador and collaborators (Salvador et al., 2018), including as response variables the following:

3.1. Dependent variables

Y₁: the grams of glucose yields per 100 grams of raw material, in order to take advantage of the cellulose composition, consists of a polysaccharide formed by β -1,4 glycosidic bonds (Cuervo et al., 2009).

For the study, the following independent variables recommended by (Salvador et al., 2018) were considered:

3.2. Independent variables

X₁: Temperature (35 °C -50 °C).

The enzymatic hydrolysis is carried out at the optimum temperature of the commercial enzyme, around 50 $^{\circ}$ C, and decreases up to 35 $^{\circ}$ C because it has been shown that these enzymes are more active in that range of temperatures (Ruegm and Tauke, 2004), (Baig et al., 2004), (Mesa, 2010).

X₂: Units of filter paper (UFP) (:10-25 UFP/g)

A cellulose concentrate (10 UFP / g of dry base) has a positive effect on hydrolysis, to

obtain better glucose yields. In addition, the literature indicates that an enzyme load of 25 UFP / g is the most indicated to achieve better glucose yields (Peñuela et al., 2007).

X₃: Agitation, in rpm (150-200 rpm).

It has been described that enzymes work much better with agitation, projecting higher glucose yield results (Mesa, 2010).

X₄: Enzymatic reaction time (15-24 hours).

Preliminary studies found good yields in a time of 24 hours (Lin et al., 2010). In addition, it is suggested that the best glucose yields are obtained in tests performed between 8 and 72 hours, having more emphasis on 24, and see how the glucose yield differs in a shorter time such as 15 hours.

X₅: Solid state in percentages (5 and 8%).

According to theoretical studies, the hydrolysis is best executed in a semi-solid state (Zhang et al., 2017). Also according to a study carried out in the analytical laboratory of renewable energy procedures of the Central University of Ecuador, provided results of glucose yields using a solids load of 2% w / v. A load of solids was maintained between 6 and 10% to achieve high yields (Peñuela et al., 2007). Other authors confirm a very acceptable glucose yield using 5% w/v (Buaban et al., 2010) (Rodrígues et al., 2014).

X₆: Use of Tween 80 surfactant, in percentages (0.1g and 0.2g).

The incorporation of commercial surfactants into the enzymatic hydrolysis stage has an effect on the increase of glucose yield up to about 20% (Mesa, 2010).

The experimental matrix of Plackett-Bürman that was proposed based on the analysis carried out for enzymatic hydrolysis with enzymatic cocktail Bacillus sp bacteria in order to determine the significance of each of the variables, is observed below:

Test/Variables	X_1	X_2	X_f	<i>X</i> ₃	X_4	X_5	X6
1	+	+	+	-	+	-	-
2	+	+	-	+	-	-	+
3	+	-	+	-	-	+	+
4	-	+	-	-	+	+	+
5	+	-	-	+	+	+	-
6	-	-	+	+	+	-	+
7	-	+	+	+	-	+	-
8	-	-	-	-	-	-	-

 Table 1.Plackett-Bürman experimental matrix

Table 2. Experimental results of glucose yield in 100g of bagasse obtained for the differe	nt
experimental responses of the 8 tests	

Test	X_1	X_2	X_f	<i>X</i> ₃	X_4	X_5	X_6	Y (g/100g)
1	1	1	1	-1	1	-1	-1	3.048
2	1	1	-1	1	-1	-1	1	0.240
3	1	-1	1	-1	-1	1	1	0.051
4	-1	1	-1	-1	1	1	1	6.307
5	1	-1	-1	1	1	1	-1	2.837
6	-1	-1	1	1	1	-1	1	0.632

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7	-1	1	1	1	-1	1	-1	11.969
8	-1	-1	-1	-1	-1	-1	-1	6.300

The results obtained in the planned experiment show that the best test is 7, which has 11.96 glucose yield per 100g of bagasse. Therefore, the conditions presented by the test for the bacteria, in relation to the factors involved for the degradation of the lignocellulosic material were the best (See Table 2).

The glucose yield coefficient for the factors studied is presented below in Table 3:

Table 3. Glucose yieldcoefficient of for the enzymatic cocktail

E_1	E_2	E_{f}	E_3	E_4	E_5	E_{6}	
-4.75	2.93	0.0042	-0.0070	-1.43	2.73	-4.23	

When implementing the design of Plackett-Bürman, by means of the coefficients of glucose yield, it is possible to observe the variables that are not significant in the experiment. This way discarding the conditions mentioned above, optimizing the enzymatic hydrolysis process.

The standard error is obtained by calculating the false estimated variables (equation 1), just as in the case of the real variables (Isaacson, 1970), thus:

$$SE = \sqrt{\frac{\Sigma(EF)^2}{No. \ offalse variables}} \tag{1}$$

The simplification of each effect is verified by comparing the tabulated value of the student's t to F/ number of false variables and the calculation of the expression 2:

$$T = \frac{E(I)}{S.E}$$
(2)

Then, if the calculated value is greater than the tabulated one, it means that the effect of the level variation of the independent variable really causes variations in the response parameter. And this is not due to experimental errors, which depends on the degree of significance of the variable, it is obtained as it is significant: P = 80, 85, 90, 95% and they are compared with the tabulated T values.

The E_3 agitation is not significant because the amount of bagasse that enters the process, when mixed with the enzymatic cocktail of bacteria, forms a cake that makes agitation difficult, this saccharification begins as a semisolid hydrolysis. Table 4 shows that Ef (false variable) and E_3 (agitation) are not significant for the experiment, the false variable is discarded.

Once condition X_3 (agitation) has been discarded, a fractional factorial design is carried out, taking into account the conditions that do influence the experiment.

3.3. Box-Hunter optimization design

Fractional factorial design 2^{5-2}) in the enzymatic hydrolysis with enzymatic cocktail of bacterium Bacillus sp, with conditions adjusted to the experimental data obtained in the laboratory are shown in Table 4:

Test	Order	X_1	X_2	X_4	X_5	X ₆
1	8	+	+	+	-	-
2	2	+	+	-	-	+
3	4	+	-	-	+	+
4	5	-	+	+	+	+
5	7	+	-	+	+	-
6	1	-	-	+	-	+
7	3	-	+	-	+	-
8	6	-	-	-	-	-

Table 4. Box-Hunter 2⁵⁻² optimization design for glucose yield

Here two relationships of the type were established:

$\mathbf{X}_5 = -\mathbf{X}_2\mathbf{X}_4,$	(3)
$X_6 = -X_1 X_2$	(4)
Then:	
$1 = -X_2 X_4 X_5,$	(5)
$1 = -X_1 X_2 X_6$	(6)
What generates the following mixing effects of the independent variables:	
$\mathbf{b}_1 = \mathbf{\beta}_1 - \mathbf{\beta}_{26} - \mathbf{\beta}_{1245},$	(7)
$\mathbf{b}_2 = \mathbf{\beta}_2 - \mathbf{\beta}_{16} \mathbf{-} \mathbf{\beta}_{45},$	(8)
$b_4 = \beta_4 - \beta_{25} - \beta_{1246},$	(9)
$\mathbf{b}_5 = \mathbf{\beta}_5 - \mathbf{\beta}_{24} - \mathbf{\beta}_{1256}$	(10)
$b_6 = \beta_6 - \beta_{12} - \beta_{2456}$	(11)

This makes it possible to ensure that the model for the estimate will have the terms corresponding to the independent variables, because the effects of the interactions are mixed with those of the independent terms.

The data adjusted for glucose yield, after replication, by means of the fractionated optimization design, taking into account the factors that influenced the enzymatic hydrolysis process, are shown in Table 5.

By discarding non-influential conditions, the costs of the processes, thus obtaining an optimization in the production.

Test	Y	Y	Y average
1	3.049	3.047	3.048
2	0.240	0.242	0.241
3	0.0513	0.052	0.051
4	6.306	6.307	6.306
5	2.837	2.838	2.837
6	0.632	0.630	0.631
7	11.969	11.970	11.969
8	6.300	6.302	6.301
Repro	ducibility	variance $\sum(Y)^2/8=$	0.000000018

Table 5. Adjusted experimental results for glucose yield in 100g of bagasse

Once the conditions that influence the experiment are considered, the average between the experiment Y' y Y'' is calculated, and then it is compared with the result obtained when solving the equation of Box-Hunter model, thus obtaining the experimental errors for each of the tests (See Tabla 5).

Table 6. Glucose yield coefficients of the enzymatic hydrolysis for the enzymatic cocktail of

 the bacterium *Bacillus* sn

the bacterium Dacinus sp					
<i>b</i> ₁	b_2	<i>b</i> ₄	\boldsymbol{b}_5	<i>b</i> ₆	
-2.37	1.46	-0.71	1.36	-2.11	

3.3.1. Box-Hunter equationmodel

 $Y = b_0 + b_1 X_1 + b_2 X_2 + b_3 X_3 + b_4 X_4 + b_5 X_5 + b_6 X_6$

(12)

test	YAverage	YEquation	Difference to the square
1	3.04	3.04	0.000026
2	0.24	0.24	0.000026
3	0.05	0.04	0.000026
4	6.30	6.30	0.000004
5	2.83	2.84	0.000026
6	0.63	0.63	0.000004
7	11.96	11.97	0.000004
8	6.30	6.29	0.000004
Adec	uation variance \sum (Yad) ² =	0.00000000091	

Table 7. Estimate results for the model of glucose yield in 100g of bagasse

With the experimental design, the reproduction variance = 0.0000000018 was calculated and with the comparison between the experiments and the estimated by the model, the adequacy test was determined by the Fisher 2 test at 8 = 0.0000000091 less than the tabulated Fisher (Perry and Chilton, 1975).

The glucose yield coefficients shown in Table 6 show the most influential variables in the experiment, these being: b_1 (Temperature) and b_6 (Tween 80) and when selecting the best test in terms of glucose yield (see Table 2), it can be concluded that the enzymatic cocktail of the bacterium *Bacillus sp*, produces a better glucose yield at a lower temperature and with less use of Tween 80.

In addition to the previous one, the remaining 24 possibilities of the design were explored with the help of the model obtained from Box-Hunter and it was determined that no other experiment would give better results.

3.4. Fermentative stage

3.4.1. Results of separate hydrolysis and fermentation (SHF).

The SHF fermentation step was carried out with the results of the test 7 which has the highest value in terms of glucose yield in 100g of bagasse. The test was carried out at 35 °C, with an enzymatic load of 25 UPF, at 200 rpm, with 6% solids and 0.1% Tween 80. The hydrolysis was carried out in a period of 15 hours and the fermentation in a period of 24 hours.

The glucose concentration values obtained in the selected test at 15 hours of enzymatic hydrolysis were 11.92 g per 100 g of bagasse, and based on the theoretical yield of 0.51 g of ethanol / g of glucose (Mesa, 2010), it was obtained that there is 6.08g of ethanol in 100g of bagasse. Then it can be concluded that 12.83kg of bagasse will be needed to produce 1 liter of ethanol, considering only the glucan fraction, and for each ton of bagasse, 77.9 liters of ethanol will be obtained.

4. CONCLUSIONS

- 1. The use of the enzymatic cocktail of native bacteria from Ecuador is an interesting proposal for the production of ethanol, since using enzymes produced with native bacteria could improve the costs of the enzymatic hydrolysis process.
- 2. The application of statistical designs will help to optimize the conditions used in laboratory experiments, which in turn will favor a future industrial scaling.
- 3. It is necessary to determine the production cost of the enzymatic cocktail of autochthonous bacteria to obtain ethanol, in this way the application in these results can be deepened.
- 4. It is important to study mixtures of autochthonous enzymes with commercial enzymes in the hydrolysis process, to analyze if glucose yields will improve.

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