

SHORT COMMUNICATION

## Influence of culture medium components on *Mycoplasma gallisepticum* growth

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**ABSTRACT:** The composition of a culture medium produced in Cuba to grow *Mycoplasma gallisepticum* was evaluated using a response surface methodology. Initially, the influence of Mycoplasma base, horse serum and yeast extract on biomass production was assessed in a 2<sup>3</sup> factorial experimental design. Then, a central composite design was applied. Mycoplasma base and horse serum factors were selected for this study. In 7 L and 35 L bioreactors, the variations carried out in the culture medium composition were estimated. The experimental results were fitted to a second order polynomial model equation. Finally, the optimal growth conditions established were at concentrations of 1,88% Mycoplasma base and 18,16% horse serum (v/v) with 0,6% of yeast extract. For the conditions tested, at a bioreactors scale, a high cellular yield of *M. gallisepticum* (higher than 0,5 ODu/mL) was obtained.

**Key words:** culture medium optimization, *Mycoplasma gallisepticum*, statistical experimental design.

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## Influencia de los componentes del medio de cultivo en el crecimiento de *Mycoplasma gallisepticum*

**RESUMEN:** Se evaluó la composición de un medio de cultivo de producción nacional para el crecimiento de *Mycoplasma gallisepticum*, utilizando la metodología de superficie de respuesta. Inicialmente se estudió la influencia de los componentes Micoplasma base, suero equino y extracto de levadura para la producción de biomasa, mediante un diseño factorial 2<sup>3</sup> y a continuación se aplicó un diseño compuesto central. Los valores de los componentes del medio de cultivo, definidos a escala de laboratorio, fueron experimentados en fermentadores de 7 L y 35 L. Los resultados del diseño compuesto central fueron ajustados en un polinomio de segundo orden, alcanzando un crecimiento óptimo a las concentraciones de 1,88% de Micoplasma base y 18,16% de suero equino (v/v) fijando el extracto de levadura en 0,6%. Se alcanzaron rendimientos celulares de *M. gallisepticum* superiores a 0,5 ODu/mL en fermentadores de 7 L y 35 L.

**Palabras clave:** optimización de medio de cultivo, *Mycoplasma gallisepticum*, diseño estadístico experimental.

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*Mycoplasma gallisepticum* (MG) is a significant respiratory and reproductive pathogen of domestic poultry (1, 2). Economic losses due to downgrading reduced feed, egg-production efficiency and medication costs have become MG infection in one of the costliest diseases faced by the poultry industry (3, 4). The current

measures to combat MG infection have included flock testing and eradication programs, as well as the use of antibiotics in both prophylactic and therapeutic application and vaccination (5, 6).

The Mollicutes (mycoplasmas) are among the most nutritionally fastidious groups of microorganisms and

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have been notoriously difficult to cultivate (7). The culture medium for the cultivation of mycoplasma species requires a complex formulation of ingredients currently regarded as essential nutrients. The most frequently used basic formulations containing a broth base, composed by beef heart infusion, peptone and other ingredients, yeast extract, glucose and sterol (animal serum), were added to this broth base.

Varela *et al.* (8) designed a broth base for MG growth which expressed good cell yields compared with commercial media for mycoplasmas like DIFCO and OXOID (9). This culture medium was used in biomass production of MG for vaccination (10).

In the field of fermentation technology, study of the culture medium is a very important aspect for improving product yield and reducing process variability, as well as for reducing the development time and overall costs (11). Due to the complexity of the culture medium and the difficulties to cultivate MG, the response surface methodology (RSM) is an approach that can be used to study the effect of several variables and to seek the better conditions for a multivariable system (12,13,14).

Therefore, the aim of this work was to study the composition of a culture medium produced in Cuba to grow MG, by using a central composite design (CCD).

The strain *M. gallisepticum* S6 (ATCC 15302), deposited in CENSA's culture collection (15), was grown in Mycoplasma broth medium (BioCen, Cuba), supplemented with horse serum and yeast extract (supplemented MBM) (8). The horse serum was supplied by LABIOFAM (Cuba), and the yeast extract was obtained from BioCen (Cuba). The horse serum was prepared by filtrating and heating for 30 minutes.

For the laboratory studies, 7,5 mL of cell suspension were inoculated into the 75 mL supplemented MBM in a 150 mL Erlenmeyer flask. This culture was incubated at 37 °C and 90 rpm for 14 h (9).

For the fermentation studies, the inoculum was introduced into 7 L and 35 L bioreactors (Chemap-Braun, Germany), containing 5 L and 30 L respectively of the supplemented MBM. The fermentation parameters controlled were: pH 7,8, temperature 37 °C, 120 rpm and 0 vvm, operated in a batch-wise mode up to 20 h of culture time in both bioreactors (9, 16).

The biomass concentration was measured by sampling the culture and reading the optical density (OD) at a wavelength of 540 nm.

The number of colonies formed (CFU) was determined by plating suitable dilutions of cultures on agar medium and the colonies counted after incubation

for 48 hours at 37°C. The procedure was performed as described in a previous paper (16). Samples were taken in duplicate every four hours.

The influence of the culture medium components was studied in shake flask experiments, specifically, the concentration of Mycoplasma base (Mb), horse serum (Hs) and yeast extract (Ye).

Factorial design: A 2<sup>3</sup> factorial experimental design and a midpoint were applied to the screening of the variables indicating where to improve yields (17). The variables (factors) were the concentrations of Mycoplasma base (X<sub>1</sub>), horse serum (X<sub>2</sub>), and yeast extract (X<sub>3</sub>) in the supplemented MBM. The cell concentration measured as OD was the response variable (Y).

The variables were tested in three coded levels: low (-1), medium (0) and high (+1). The coded values corresponded for the variables as follows: X<sub>1</sub>: -1 (20 g/L), 0 (25 g/L), +1 (30 g/L); X<sub>2</sub>: -1 (160 mL/L), 0 (200 mL/L), +1 (240 mL/L); X<sub>3</sub>: -1 (6 g/L), 0 (10 g/L), +1 (14 g/L). The midpoint (coded value 0) corresponded to the quantities commonly used (Control).

Central Composite Design: Once the direction improving yields was known, a star design (with the coded value  $\alpha = \pm 1,682$ ) (18) was performed to determine a better statistical model which described the relationship between the variables Mb and Hs. The variable yeast extract was kept fixed at the value indicated in the factorial design. The levels studied in the CCD are shown in Table. The X value for  $\alpha$  (X <sub>$\alpha$</sub> ) was calculated for the equation:

$$\alpha = \frac{X_{\alpha} - \bar{X}}{\frac{\Delta X}{2}}$$

Where:

$\bar{X}$  15 g/L and 120 mL/L for X<sub>1</sub> and X<sub>2</sub> respectively  
 $\frac{\Delta X}{2}$  5 g/L and 40 mL/L for X<sub>1</sub> and X<sub>2</sub> respectively

For calculating the optimal point, a second order polynomial equation was fitted to the experimental results of CCD as it represented the behavior of such a system more appropriately.

This equation was:

$$Y = \beta_0 + \beta_1 X_1 + \beta_2 X_2 + \beta_1 \beta_1 X_1^2 + \beta_2 \beta_2 X_2^2 + \beta_1 \beta_2 X_1 X_2$$

Where Y was the response variable (DO),  $\beta_0$  the intercept/constant,  $\beta_1$  and  $\beta_2$  the linear coefficients,

**TABLE.** Levels of factors used in the CCD./ *Niveles de los factores utilizados en el DCC*

Runs	X <sub>1</sub> : Mycoplasma base coded value (quantity in g/L)	X <sub>2</sub> : Horse serum coded value (quantity in mL/L)
1	1 (20)	-1 (80)
2	-1 (10)	1 (160)
3	1 (20)	1 (160)
4	-1 (10)	-1 (80)
5	1,682 (23,41)	0 (120)
6	-1,682 (6,59)	0 (120)
7	0 (15)	1,682 (187,28)
8	0 (15)	-1,682 (52,72)
9	0 (15)	0 (120)

$\beta_1\beta_1$  and  $\beta_2\beta_2$  the squared/quadratic coefficients,  $\beta_1\beta_2$  the interaction coefficients, and  $X_1$ ,  $X_2$ ,  $X_1^2$ ,  $X_2^2$  and  $X_1X_2$  were the levels of the independent variables.

Runs were performed in triplicate. The whole statistical procedure of the experimental designs was carried out with the software package Statgraphics Plus® for Windows 5.1 and Microsoft Office Excel software. The quality of the fitness of the polynomial model equation was expressed by the coefficient of determination  $R^2$ , and the significance was defined as  $p < 0,05$ .

The biotechnological production process is the result of time-consuming and expensive research and development. For most favorable returns, it is necessary to improve the culture medium, the producer strain and other process parameters to reach a maximal productivity or the highest production capacity (19).

**Factorial design:** Due to the complexity of the culture medium for growing MG, a RSM was conceived to determine the most favorable composition of the medium for the microorganism growth. In the initial step, a  $2^3$  factorial design served as a test to identify the effect of the concentration of Mb, Hs and Ye on MG yields, which indicated that the variable Hs and its interaction with the variables Mb and Ye were not significant in the region studied ( $p < 0,05$ ). The direction of the highest yields was obtained with lower concentrations of Mb and Ye.

**Central Composite Design:** A CCD was used to continue this study. Lower concentrations of Mb and Hs were used; additionally, Ye concentration was kept at 6 g/L.

A multiple regression analysis was performed with the result that, in this region, the two variables (Mb and Hs) evaluated and their quadratic interactions were significant, and the mathematical model represented was:

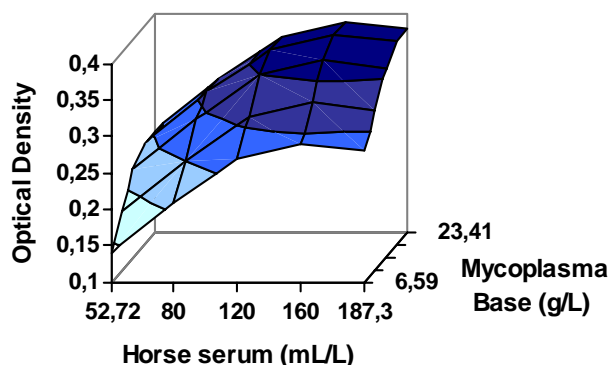
$$OD = 0,350 + 0,029X_1 + 0,040X_2 - 0,019X_1^2 - 0,013X_2^2$$

$$R^2 = 0,9265$$

$$p_{\text{model}} = 0,0$$

Where  $X_1$  and  $X_2$  represent the coded levels of Mb and Hs, respectively.

As it can be seen, the statistical model obtained was significant and indicated that the equation could explain 92,65% of the response variability. The optimum of these two variables in the region studied corresponded to 18,8 g/L of Mb and 181,6 mL/L of Hs using 6 g/L of Ye. The effect of the culture medium concentration on cell concentration is shown in Figure 1.



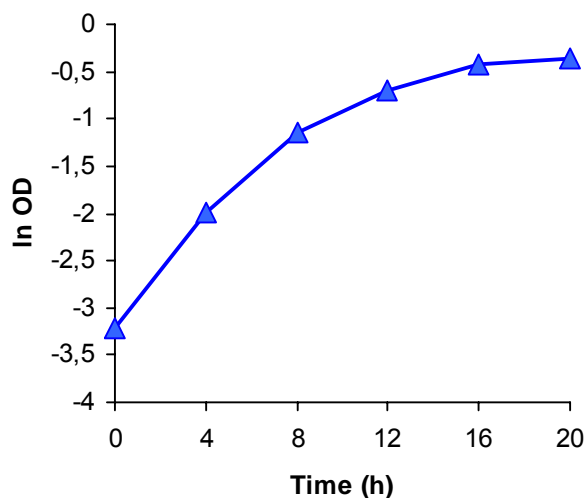
**FIGURE 1.** Surface response obtained in function of the variables Mycoplasma base and horse serum./ *Superficie de respuesta obtenida en función de las variables Micoplasma base y suero equino.*

The RSM applied for this statistical study had been used for several purposes including medium optimization, metabolites production and extraction conditions. Previously, Pérez *et al.* (20) studied the culture medium for growing MG produced by OXOID (England) by using this methodology, which had no effect on the expression of antigen proteins, but the yields were low compared with the present work.

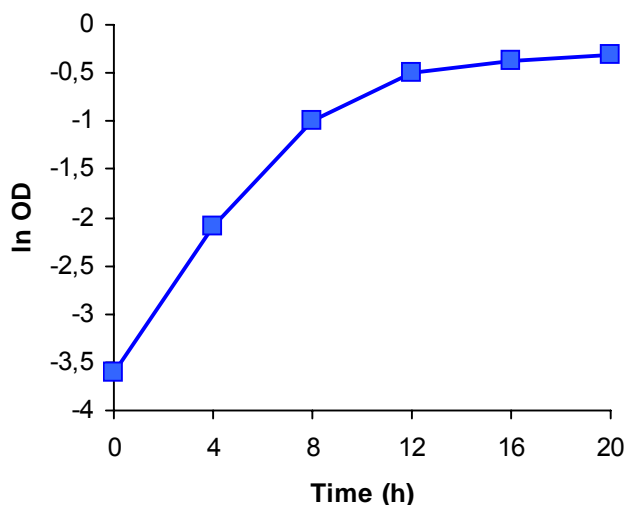
Hwang *et al.* (13) reported that the culture medium composition for biomass production of *M. hyopneumoniae* was optimized by means of the RSM. They confirmed that fresh yeast extract, horse serum and porcine serum were the major factors influencing mycoplasma protein production. Other authors (21) increased the Human Epidermal Growth Factor expression levels and reduced their degradation rate by optimizing the culture conditions. In other case, Ruiz *et al.* (22) established a method for obtaining pharmaceutical grade plasmid DNA from *Escherichia coli* culture together with an optimized purification process.

In order to confirm whether the results obtained by the model could be experimentally reproduced, MG was grown using these conditions (modified supplemented MBM), and cell concentration values of  $0,459 \pm 0,050$  OD units were reached.

The modified supplemented MBM has been proven in batch fermentation with bioreactors. The growth kinetics in bioreactors 7 and 35 L are represented in Figures 2 and 3 respectively.



**FIGURE 2.** MG growth in 7 L fermenter./ *Crecimiento de MG en fermentador de 7 L.*



**FIGURE 3.** MG growth in 35 L fermenter./ *Crecimiento de MG en fermentador de 35 L.*

During the first 8 hours of growth, a considerably increase of the optical density was observed. Figures 2 and 3 show that this medium reached the end of the exponential growth phase between 8 and 12 hours with a value of the specific growth rate ( $\mu$ ) of  $0,262 \pm 0,002$   $\text{h}^{-1}$  in the 7 L bioreactor at 12 hours, which corresponded to a cell yield of  $0,599 \pm 0,006$  OD units and  $6.10^{10} \pm 0,48$  CFU/mL, higher than ( $p < 0,05$ ) what was obtained with the culture medium before applying the experimental optimization techniques (16). In the 35 L bioreactor at 12 hours, the specific growth rate was  $0,213 \pm 0,02$   $\text{h}^{-1}$  with cell yields of  $0,514 \pm 0,015$  OD units and  $5,8.10^{10} \pm 0,43$  CFU/mL, yields similar to those obtained at the scale of 7 L.

In summary, the composition of a Cuban culture medium for MG growth was studied with a significant impact on increasing the biomass production at a laboratory or larger scale fermentation process with lower costs.

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